

xxvi Nomenclature

X_m	mole fraction of functional group m in UNIFAC method	y	mole fraction in vapor phase; distance; mass fraction in extract; mass fraction in overflow
x	mole fraction in liquid phase; mole fraction in any phase; distance; mass fraction in raffinate; mass fraction in underflow; mass fraction of particles	\mathbf{y}	vector of mole fractions in vapor phase
x'	normalized mole fraction $= x_i / \sum_{j=1}^C x_j$	Z	compressibility factor $= Pv/RT$; total mass; height
\mathbf{x}	vector of mole fractions in liquid phase	Z_f	froth height on a tray
x_n	fraction of crystals of size smaller than L	Z_L	length of liquid flow path across a tray
Y	mole or mass ratio; mass ratio of soluble material to solvent in overflow; pressure-drop factor for packed columns defined by (6-102); concentration of solute in solvent; parameter in (9-34)	\bar{Z}	lattice coordination number in UNIQUAC and UNIFAC equations
		z	mole fraction in any phase; overall mole fraction in combined phases; distance; overall mole fraction in feed; dimensionless crystal size; length of liquid flow path across tray
		\mathbf{z}	vector of mole fractions in overall mixture

Greek Letters

α	thermal diffusivity, $k/\rho C_p$; relative volatility; surface area per adsorbed molecule	Λ_{ij}	binary interaction parameter in Wilson equation
α^*	ideal separation factor for a membrane	λ	mV/L ; radiation wavelength
α_{ij}	relative volatility of component i with respect to component j for vapor-liquid equilibria; parameter in NRTL equation	λ_+, λ_-	limiting ionic conductances of cation and anion, respectively
$\alpha_j, \beta_j \gamma_j$	energy-balance parameters defined by (10-23) to (10-26)	λ_{ij}	energy of interaction in Wilson equation
β_{ij}	relative selectivity of component i with respect to component j for liquid-liquid equilibria	μ	chemical potential or partial molar Gibbs free energy; viscosity
Γ	film flow rate/unit width of film; thermodynamic function defined by (12-37)	ν	momentum diffusivity (kinematic viscosity), μ/ρ ; wave frequency; stoichiometric coefficient
Γ_k	residual activity coefficient of functional group k in UNIFAC equation	$\nu_k^{(i)}$	number of functional groups of kind k in molecule i in UNIFAC method
γ	specific heat ratio; activity coefficient	ξ	fractional current efficiency; dimensionless distance in adsorption defined by (15-115); dimensionless warped time in (11-2)
Δ	change (final – initial)	π	osmotic pressure; product of ionic concentrations
δ	solubility parameter; film thickness; velocity boundary layer thickness; thickness of the laminar sublayer in the Prandtl analogy	ρ	mass density
δ_c	concentration boundary layer thickness	ρ_b	bulk density
δ_{ij}	Kronecker delta	ρ_M	crystal density
ϵ	exponent parameter in (3-40); fractional porosity; allowable error; tolerance in (10-31)	ρ_p	particle density
ϵ_b	bed porosity (external void fraction)	ρ_s	true (crystalline) solid density
ϵ_D	eddy diffusivity for diffusion (mass transfer)	σ	surface tension; interfacial tension; Stefan-Boltzmann constant $= 5.671 \times 10^{-8} \text{ W/m}^2 \cdot \text{K}^4$
ϵ_H	eddy diffusivity for heat transfer	σ_I	interfacial tension
ϵ_M	eddy diffusivity for momentum transfer	$\sigma_{s,L}$	interfacial tension between crystal and solution
ϵ_p	particle porosity (internal void fraction)	τ	tortuosity; shear stress; dimensionless time in adsorption defined by (15-116); retention time of mother liquor in crystallizer; convergence criterion in (10-32)
η	Murphree vapor-phase plate efficiency in (10-73)	τ_{ij}	binary interaction parameter in NRTL equation
θ	area fraction in UNIQUAC and UNIFAC equations; dimensionless concentration change defined in (3-80); correction factor in Edmister group method; cut equal to permeate flow rate to feed flow rate for a membrane; contact angle; fractional coverage in Langmuir equation; solids residence time in a dryer; root of the Underwood equation, (9-28)	τ_w	shear stress at wall
θ_L	average liquid residence time on a tray	ν	number of ions per molecule
κ	Maxwell-Stefan mass-transfer coefficient in a binary mixture	Φ, Φ'	volume fraction; parameter in Underwood equations (9-24) and (9-25)
		$\bar{\Phi}$	local volume fraction in the Wilson equation
		$\phi\{t\}$	probability function in the surface renewal theory
		ϕ	pure-species fugacity coefficient; association factor in the Wilke-Chang equation; recovery

	factor in absorption and stripping; volume fraction; concentration ratio defined by (15-125)		equilibria calculations for single-stage extraction; sphericity defined before Example 15.7
$\bar{\Phi}$	partial fugacity coefficient	Ψ_o	dry-packing resistance coefficient given by (6-113)
Φ_{df}	froth density	Ψ	fractional entrainment; loading ratio defined by (15-126); sphericity
Φ_e	effective relative density of froth defined by (6-48)	ω	acentric factor defined by (2-45); segment fraction in UNIFAC method
Φ_s	particle sphericity		
Ψ	segment fraction in UNIQUAC equation; V/F in flash calculations; E/F in liquid-liquid		

Subscripts

A	solute	L	liquid phase; leaching stage
a, ads	adsorption	LM	log mean of two values, A and $B = (A - B)/\ln(A/B)$
avg	average	LP	low pressure
B	bottoms	M	mass transfer; mixing-point condition; mixture
b	bulk conditions; buoyancy	m	mixture; maximum
bubble	bubble-point condition	max	maximum
C	condenser; carrier; continuous phase	min	minimum
c	critical; convection; constant-rate period	N	stage
cum	cumulative	n	stage
D	distillate, dispersed phase; displacement	O	overall
d	drag; desorption	$o, 0$	reference condition; initial condition
d, db	dry bulb	out	leaving
des	desorption	OV	overhead vapor
dew	dew-point condition	P	permeate
ds	dry solid	R	reboiler; rectification section; retentate
E	enriching (absorption) section	r	reduced; reference component; radiation
e	effective; element	res	residence time
eff	effective	S	solid; stripping section; sidestream; solvent; stage; salt
F	feed	s	source or sink; surface condition; solute; saturation
f	flooding; feed; falling-rate period	T	total
G	gas phase	t	turbulent contribution
GM	geometric mean of two values, A and $B = \text{square root of } A \text{ times } B$	V	vapor
g	gravity	W	batch still
gi	gas in	w	wet solid-gas interface
go	gas out	w, wb	wet bulb
H, h	heat transfer	ws	wet solid
I, I	interface condition	X	exhausting (stripping) section
i	particular species or component	x, y, z	directions
in	entering	δ	at the edge of the laminar sublayer
irr	irreversible	0	surroundings; initial
j	stage number	∞	infinite dilution; pinch-point zone
k	particular separator; key component		

Superscripts

E	excess; extract phase	LF	liquid feed
F	feed	o	pure species; standard state; reference condition
ID	ideal mixture	p	particular phase
(k)	iteration index		