

Basic Concepts (Engineering & Science)

$g_c = ma/F$

SI: $1 \text{ kg} \cdot \text{m} / (\text{N} \cdot \text{s}^2)$
 ENG: $32.174 \text{ lbm} \cdot \text{ft} / (\text{lb}_f \cdot \text{s}^2)$

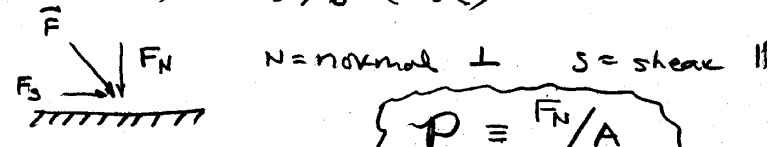
Work = $W = F \cdot d$
 Power = $P = dW/dt$

$J \equiv \text{N} \cdot \text{m}$ $\text{W} = \text{J}/\text{s}$
 $\text{hp} = 550 \text{ ft} \cdot \text{lb}_f / \text{s}$
 $\text{btu} = 778.16 \text{ ft} \cdot \text{lb}_f$

$\hat{V} = 22.4 \text{ L} / \text{g} \cdot \text{mole}$ @ 0°C , 1 atm (101.3 kPa)
 $= 359 \text{ ft}^3 / \text{lb} \cdot \text{mole}$ @ 32°F , $14.69 \text{ lb}_f / \text{in}^2$

Circle: $\pi D^2 / 4$ (area) πD (circum)
 Sphere: πD^2 (surf area) $\pi D^3 / 6$ (vol)

Fluid Statics



$N = \text{normal} \perp$ $S = \text{shear} \parallel$

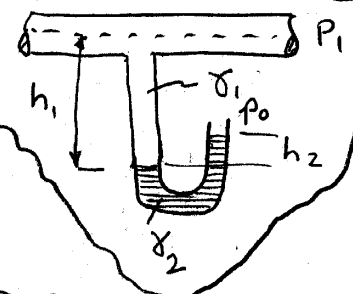
$P \equiv F_N / A$
 $\tau \equiv F_S / A$

I.G.L. $PV = nRT$ $V/n = \bar{V}$

Hydrostatic Eg. $\Delta P = \rho g \Delta h$ $P = f(z)$ only
 (spec. gravity) $\gamma = \frac{\rho g}{g_c}$ $\therefore \Delta P = \gamma \Delta h$
 (density) ρ

Water @ 4°C $\rho = 62.39 \text{ lb}/\text{ft}^3$ ($1000 \text{ kg}/\text{m}^3$)
 $\gamma = 62.39 \text{ lb}_f/\text{ft}^3$ ($9860 \text{ N}/\text{m}^3$)

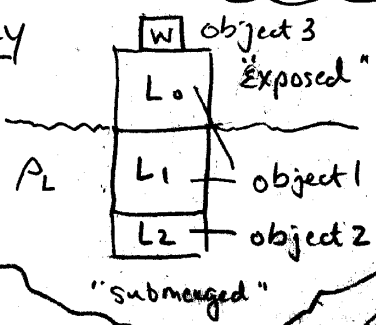
Manometry



$P_0 = P_1 + \gamma_1 h_1 - \gamma_2 h_2$

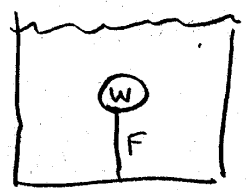
$P_{\text{abs}} = P_{\text{gage}} + P_{\text{ref}}$ ← usually 1 atm
 $h = \frac{\Delta P}{\gamma} = \frac{\Delta P g_c}{\rho g}$ (head)

Bouyancy



$\Delta V = \Delta h A$ (vol disp)
 $W + \gamma_2 L_2 A + A(L_1 + L_0) \gamma_1 = (L_1 + L_2) A \gamma_L$
 $W_{\text{obj}} = W_{\text{H}_2\text{O displaced}}$

Tethered objects and Submerged



$W_{\text{H}_2\text{O disp}} = W_{\text{obj}} + F_{\text{drain}}$
 $W_{\text{app}} = W_{\text{obj}} - W_{\text{H}_2\text{O}}$

apparent wt

Statics con't

kinematic viscosity $\nu = \mu / \rho$

Properties of matter:

$$\begin{aligned} \mu_{\text{gas}} &\uparrow \text{ as } T \uparrow \\ \mu_{\text{liq}} &\downarrow \text{ as } T \uparrow \end{aligned}$$

Dimensional Analysis

"Buckingham Pi Theorem"

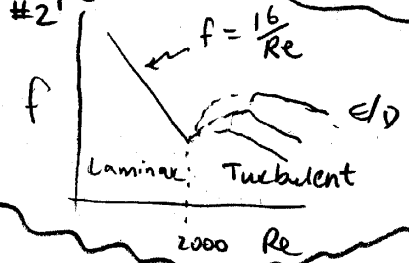
$n = \#$ of quantities of interest
 $m = \#$ of indep. variables (T, P etc) ...

$\# \pi\text{'s} = n - m$ ($m=3$ no T dependence
 $m=4$ w/ T dependence)

Example: Hagen Poiseuille Eq. (Laminar)

#1 $Q = (\pi/128) \frac{\Delta P}{L} (D^4/\mu)$ $n=4$ ($\Delta P/L, D, \mu, Q$)
 $\therefore n-m = 4-3 = 1$ Pi group.

Example: #2



$n=6$ $f, \Delta P/L, D, \rho, v^2, \epsilon$
 $m=3$ $6-3=3$
 $\pi_1 = f$ $\pi_2 = N_{Re}$ $\pi_3 = \epsilon/D$

Modeling & Similitude

Form dimensionless numbers from ratios of forces.

$F_I = \text{inertia}$	$\rho L^2 v^2$	} $F_I/F_v = N_{Re} = Dv\rho/\mu$
$F_g = \text{gravity}$	$\rho g L^3$	
$F_v = \text{viscous}$	$\mu L v$	
$F_p = \text{pressure}$	$\Delta P (L^3)$	
$F_{ST} = \text{surf tension}$	σL	
$F_c = \text{compressibility}$	$k L^2$	

$N_{Fr} = v/\sqrt{Lg}$
 $N_{Mach} = v/\sqrt{\gamma k p}$
 $N_{Weber} = v/\sqrt{\sigma/\rho L}$

Phenomenological Models

Case I - $N_{Re} = Dv\rho/\mu = Lv\rho/\mu$ "Enclosed flow", pipes, conduits, flow notes, fans, pumps, turbines, "Fully immersed flow" Autos, submarines, buildings.

Case II Gravity waves $N_{Fr} = v/\sqrt{Lg}$ or v^2/Lg
 Ships hulls or open channel flow

Case III $N_{We} = v/\sqrt{\sigma/\rho L}$ surface tension, capillary tubes, wicking, heat pipes

Case IV Drag forces $C_D = F_D/(\rho v^2/2A)$ includ. parachutes.

Common dimensions.

$$Q = L^3/\theta^{-1} \quad \mu = ML^{-1}\theta^{-1}$$

$$\Delta p = ML^{-1}\theta^{-2} \quad F = ML\theta^{-2}$$

$$n = \theta^{-1} \quad \sigma = M\theta^{-2}$$

$$\gamma = ML^{-3} \quad \nu = L^2\theta^{-1}$$

Reynolds Transport Thm

$$\frac{dB}{dt}\bigg|_{sys} = \frac{d}{dt} \int_{CV} \beta \rho dV + \int_{CS} \beta \rho \vec{v} \cdot d\vec{A}$$

Mass Continuity

$B = m \quad \beta = B/m = 1$

Yields: $\dot{m} = \int_A \rho \vec{v} \cdot d\vec{A}$

$\bar{V} = \dot{m}/\rho A \quad Q = \bar{V}A = \dot{m}/\rho$

$\therefore \dot{m} = \rho \bar{V}A = \text{const}$

also $G = \bar{V}\rho = \frac{\dot{m}}{A} = \text{mass flux}$

At ss. $\dot{m}_{in} = \dot{m}_{out}$

Energy Eq.

$B = E \quad \beta = E/m = e$

Yields: $\frac{dE}{dt}\bigg|_{sys} = \frac{d}{dt} \int_{CV} e \rho dV + \int_{CS} e \rho \vec{v} \cdot d\vec{A}$ w/ $e = e_{int} + e_{KE} + e_{PE}$
and note: $\dot{W} = \vec{F} \cdot \vec{v}$

(1) $\therefore \dot{Q} - \dot{W}_s = \dot{m} \left[\alpha \frac{\hat{V}^2}{2} + gz + h \right]_{out} - \dot{m} \left[\alpha \frac{\hat{V}^2}{2} + gz + h \right]_{in}$ (@ ss)

where $\alpha \approx 1.05$ turb (cic pipe)
 $\alpha = 2.00$ lam (")

↑ work units

Divide (1) by $\dot{m}g$

(2)

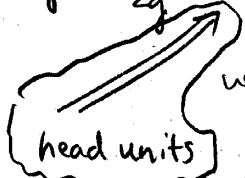
$$\frac{P_1}{\rho} + \alpha \frac{\hat{V}_1^2}{2} + z_1 g + h_p = \frac{P_2}{\rho} + \alpha \frac{\hat{V}_2^2}{2} + z_2 g + h_t + h_L$$

↑ KE units

where $h_p = \frac{\dot{W}}{mg} = \frac{\dot{W}}{Q\rho g} = \frac{\dot{W}}{Q\gamma}$

or also (3)

$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + z_1 + h_p(\eta) = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_t + h_L$$



where $W_p = W_s(\text{shaft}) / \eta$

Conversion Factors & Phys Properties:

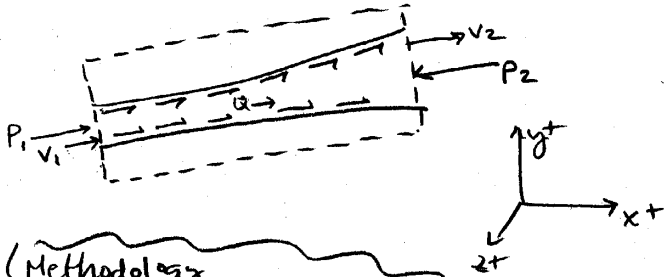
- Power = hpump (in)
- 7.48 lb = 1 gallon
- 1 atm = 33.90 ft-H₂O
- HP = 550 ft.lbf/s
- J = N.m = kg m²/s²
- 6.895 x 10⁸ N/m² = PSI
- 1 ft.lbf = 1.356 J
- Btu = 778.16 ft.lbf
- Btu = 1055.06 J
- hp = 0.7457 kW
- 1 ft.lbf/lbm = 2.989 J/kg
- W = J/s
- J/s (ρ) = J/kg (sp energy)
- h = u + pv

Momentum Eq

$B = m\vec{v} \quad \beta = \vec{v}$

yields: $\frac{d(m\vec{v})}{dt}_{sys} = \sum \vec{F} = \frac{d}{dt} \int_{CV} \vec{v} \rho dV + \int_{CS} \vec{v} \rho \vec{v} \cdot d\vec{A}$

where $\sum \vec{F} = F_N + F_B + F_S + F_e = \sum \vec{m}_{out} - \sum \vec{m}_{in}$



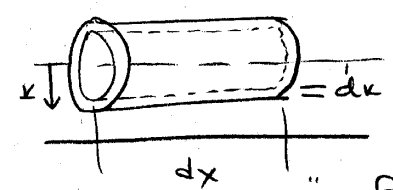
$\sum \vec{m}_{out} - \sum \vec{m}_{in}$

- $F_N = \text{normal} = P \cdot A$ pressure
- $F_S = \text{shear} = \tau A$ shear
- $F_B = \text{body} = mg$ grav (wt)
- $F_e = \text{external (all other)}$

Methodology

1. Always draw CV. Stay outside to avoid shear.
2. Specify coord system
3. Use gage pressures
4. Pick ext force direction arbitrarily (+ = right - = wrong assumption)
5. Remember trig & keep all angles $\leq 90^\circ$

Circular pipe (laminar)



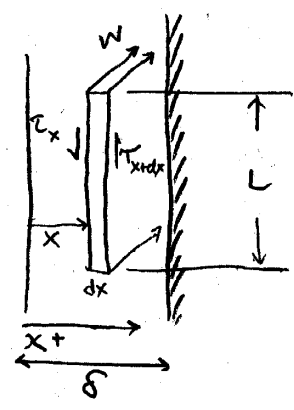
$F_p = P_x A_x + P_{x+dx} A_{x+dx}$ (trig)
 $F_e = 0$
 $F_s = \tau_{xx} (2\pi r) dx - \tau_{(x+dx)} (2\pi r) dx$

Cir. pipe results

$\tau_{rx} = \frac{\Delta P}{L} \frac{r}{2} \quad \tau_{rx} = -\mu \frac{\partial v_x}{\partial r}$

$\bar{v}_x = (P_o - P_L) D^2 / 32 \mu L$
 $v_{max} = (P_o - P_L) R^2 / 4 \mu L$

Falling Film (laminar)
 [fully developed]



$F_p = P_o A_o - P_L A_L$
 $F_s = \tau_x LW - \lambda_{x+dx} LW - \frac{\partial \tau}{\partial x} dx LW$
 $F_B = (\delta x LW) \rho g$
 $F_e = 0$

Falling Film Results

$\Gamma = m/t \cdot l = \dot{m}/l$
 $Re = \frac{4\Gamma}{\mu} = 4\rho \delta v_z / \mu$

$\hat{v}_z = \rho g \delta^2 / 3\mu$
 $\hat{v}_z = 2/3 v_{z,max}$